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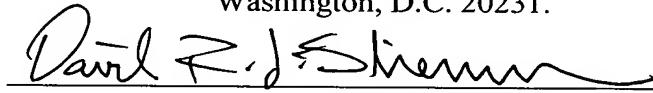
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For: Method and Apparatus for Mixing Dilution Liquid into a Stock Flow in a Paper or Board Machine

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TITLE OF THE INVENTION

Method and Apparatus for Mixing Dilution Liquid into a Stock Flow in a Paper or Board Machine

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CROSS REFERENCES TO RELATED APPLICATIONS

This application is a U.S. national stage application of PCT Application No. PCT/FI00/00320, filed 14 April 2000, and claims priority on Finnish Application No. 990967, filed April 28, 1999, the disclosures of both of which applications are incorporated by reference herein.

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**STATEMENT AS TO RIGHTS TO INVENTIONS MADE UNDER
FEDERALLY SPONSORED RESEARCH AND DEVELOPMENT**

Not applicable.

BACKGROUND OF THE INVENTION

The invention relates to a method and an apparatus for mixing dilution liquid into a stock flow in a paper or board machine.

With respect to the prior art, we refer to the publications DE 19723861 and FI
5 901593.

It has become clear that with the development of measuring devices on the market ever higher requirements are set for the accuracy of control of the basis weight profile. Today, the dilution spacing in a so-called dilution headbox is about 32-75 mm, and it is not possible to reduce it any more if fibre-containing white water is
10 used as dilution water, because dilution feed ducts which remain open by means of white water cannot be accommodated between tube rows with a dense spacing.

SUMMARY OF THE INVENTION

As a solution it is proposed that, when needed, dilution is changed to comprise two stages such that coarse control is carried out by means of white water and fine
15 control is carried out by means of raw water.

The increasing requirement of control accuracy calls for an increasingly denser dilution spacing and, therefore, still narrower dilution feed ducts. If white water is used as dilution water, narrow dilution ducts clog easily. Clogging problems are not encountered with raw water, but its "full-scale use" is not economical and sensible
20 for environmental reasons.

The idea of the two-stage dilution is to correct large basis weight profile errors by a large amount of white water and small profile errors by a small amount of raw water. A good raw water economy is achieved by this means in a paper mill. Another benefit of the two-stage arrangement is the good possibility of adjusting the basis
25 weight profile. The entire valve control area can be made use of and control valves of an optimum size can be selected for both control operations.

Coarse control is carried out in a tube bank after an inlet header, as in the conventional headbox. In the first dilution stage, the control spacing can be increased, for example, to 120 mm such that one dilution member feeds two tube rows. Coarse control corrects major errors in the shape of the profile, such as, for example, profile errors arising from web shrinkage. The small errors which remain in the profile after coarse control are rectified by means of fine control dilution in the second stage.

Fine adjustment is carried out as turbulence generator dilution by supplying some or each of the tubes of the turbulence generator with dilution liquid. A very small amount of dilution liquid is needed for rectifying the remaining small errors, so raw water or clarified white water obtained from a fibre recovery unit can be used economically as dilution water in fine control. Since, for example, raw water does not contain contaminating or clogging particles, the dilution ducts can be provided in very narrow spaces. Moreover, the control valves and the actuators operating the valves can be ordinary standard devices available on the market, which devices are considerably less expensive than conventional dilution valves and actuators.

Minimum local dilution with raw water can be almost 0 % and maximum local dilution need not be high because the consistency of raw water is 0 % and the remaining error to be corrected is small. Thus, the amount of the more expensive raw water consumed is very small. No separate circulation is required for the feed of raw water.

The price of the arrangement disclosed hardly differs at all from the price of the conventional dilution headbox. The proposed arrangement uses half the number of expensive dilution valves and actuators.

Thus, mixing units are prior known in which dilution water and stock passed from the inlet header of the headbox are mixed and the combined flow is passed further onwards in the headbox and onto a forming wire. Points of supply of dilution liquid

are situated in different positions of width across the headbox and, thus, depending on the density of the dilution points placed across the width of the headbox, desired resolution is obtained for control of the basis weight of the web.

Thus, this application proposes using dilution in at least two stages. Coarse control of the basis weight profile is carried out in the first stage of dilution and fine control is carried out in the second stage of dilution. White water is used as dilution water in the first stage and the valves are arranged with a less dense spacing in the first stage than in the second control stage in which the valves are arranged with a denser spacing than in the first dilution stage. An advantage of the arrangement is that the valves of the second stage can have a construction that demands less precision and thus be less expensive than the valves of the first stage. They do not clog because fibre-free dilution water is used in the second stage. The valves can thus contain smaller ducts. They do not demand much space.

Within the scope of the invention, it is also possible to use control with three or more stages, but the most advantageous control arrangement is two-stage adjustment of the dilution liquid.

The headbox structure of the paper or board machine can advantageously be as follows:

- a) stock is passed into a stock inlet header which tapers towards its outlet end in a conventional manner,
- b) the stock flow is passed from the stock inlet header into a tube bank and further through the tube bank into an intermediate chamber,
- c) the stock flow is passed from the intermediate chamber further into a turbulence generator and from the turbulence generator further through a slice cone onto a forming wire.

In the following, the invention will be described with reference to some

advantageous embodiments of the invention shown in the figures of the accompanying drawings, to which the invention is, however, not intended to be exclusively confined.

BRIEF DESCRIPTION OF THE DRAWINGS

5 FIG. 1A is a graph showing uncorrected basis weight profile of stock passed from an inlet header J_1 across the width of the machine.

FIG. 1B is a graph showing a basis weight profile after the valves $V_1, V_2 \dots$ controlling the basis weight profile.

10 FIG. 1C is a graph showing a corrected basis weight profile of stock after the second dilution stage.

FIG. 2 shows a headbox of a paper or board machine in accordance with the invention.

DESCRIPTION OF THE PREFERRED EMBODIMENTS

In accordance with the invention, the valves of the first dilution stage are located in connection with the tube bank and the valves of the second dilution stage are located after the intermediate chamber in connection with the turbulence generator.

Figures 1A--1C show the method according to the invention in stages. The graph F_1 , in Fig. 1A represents an uncorrected basis weight profile of stock passed from an inlet header J_1 across the width of the machine. In the first dilution stage, coarse 20 control of the basis weight profile is carried out by means of valves $V_1, V_2 \dots$ of the first dilution stage.

The graph F_1' in Fig. 1B shows a basis weight profile after the valves $V_1, V_2 \dots$ controlling the basis weight profile.

In Fig. 1C, the graph F_2 shows a corrected basis weight profile of stock after the second dilution stage. Dilution valves V_1' , V_2' ... of the second dilution stage are placed, for example, in connection with a turbulence generator. The graph F_2 shows the basis weight profile in the stock flow across the width of the machine after adjustment carried out by the valves V_1' , V_2' ... of the second stage.

In Figs. 1A--1C, the horizontal coordinate X represents headbox operation and the vertical coordinate Y represents the basis weight. A basis weight deviation from the zero level, i.e. a basis weight error, occurring in the stock and further in the web can be read from the vertical coordinate Y. The basis weight profile can be measured from the stock flow, but the easiest way to measure the basis weight is to measure it from a finished paper or board web.

Figure 2 shows a headbox of a paper or board machine in accordance with the invention.

In Fig. 1A, the first graph F_1 shows control in the first dilution stage. The graph F_1 depicts a basis weight variation which occurs in the stock before the control valves V_1, V_2, V_3 ... of the first stage.

In Fig. 1A, the graph F_1 shows a basis weight variation which occurs in the stock M_1 . An average basis weight variation is further shown by the graph F_{10} . As seen in the graph F_{10} , in the basis weight there is firstly a shape error and secondly a local error. Said shape error is corrected by means of the control valves V_1, V_2 ... the first dilution stage I such that the graph F_{10} becomes straight. The local errors are rectified by means of the control valves V_1', V_2' ... in the basis weight adjustment of the second stage II.

The graph F_1' of Fig. 1B illustrates the situation after the first stage, in which connection control of the basis weight of the stock M_1 has been accomplished by introduction of dilution liquid. In the graph, the horizontal coordinate X represents

the cross-direction position of the headbox and the positions of the valves are denoted with V_1' , V_2' , V_3' ... in the horizontal coordinate X. The vertical coordinate Y shows a basis weight error of the stock after the adjustment of the first stage I.

Fig. 1C shows the basis weight control of the second dilution stage II. The graph F_2 illustrates the situation after the dilution liquid valves V_1' , V_2' , V_3' ... of the second dilution stage. The graph F_2 is straight and there does not occur any basis weight error any more. In the graph, the horizontal coordinates represent the width of the headbox, and the position of the valves is denoted with V_1' , V_2' ... at each particular point of the horizontal coordinate X. The vertical coordinate Y shows the basis weight error of the stock. The zero level illustrates a correct constant basis weight situation. White water is used as dilution water in the first stage I, which water may contain fibres and fines/fillers. The dilution of the second stage II is carried out by means of dilution water which does not contain fibres, such as raw water. A benefit in that case is that conventional valves V_1' , V_2' , V_3' ... can be used because there is no risk of the ducts being clogged by fibres.

The dilution water feeds of the kind mentioned can be placed with a denser spacing than those of the current arrangements, the spacing between the valves in dilution control can be reduced from 60 mm to 30 mm. The amount of the dilution water used is small and there is no need for a separate circulation of the dilution water. Consequently, the construction of the arrangement according to the invention is advantageous and it allows a denser spacing to be used between the valves, i.e. higher resolution, i.e. a higher accuracy of control. By using raw water in the adjustment of the second stage it is possible to employ conventional valve arrangements, in which connection the valves can also be placed with a spacing of even 20-30 mm with respect to one another, whereas in the adjustment of the first stage, the control resolution can be changed in the case of said stage so that the valves are disposed, for example, with a spacing of 120 mm with respect to one another instead of, for example, conventional single-stage dilution of 60 mm. Thus, by using the arrangement in accordance with the invention in which the dilution of the first stage employs white water as dilution water and the dilution of the second

stage employs fibre-free dilution water, an overall end result is achieved in which the accuracy of control is better than in conventional single-stage dilution and in which the construction costs with respect to structure have, however, not increased as compared with single-stage dilution.

5 The coarse control of the basis weight profile is carried out in the first stage of dilution and the fine control thereof is carried out in the second stage of dilution. The dilution water used in the second dilution stage is advantageously raw water or clarified white water. Thus, the dilution water of the second stage contains solids and/or fibres substantially less in percentage terms than the dilution water of the first
10 stage, which is advantageously water taken out of the wire. Most advantageously, the dilution water of the second stage is raw water that does not contain any solids and fillers and fibres.

Fig. 2 shows a headbox 10 of a paper or board machine in accordance with the invention. The headbox comprises a stock inlet header J_1 , a tube bank 11 after the stock inlet header, an intermediate chamber 12 after the tube bank, and a turbulence generator 13 after the intermediate chamber, and further a slice cone 14 from which stock M_1 is passed onto a forming wire H_1 . In accordance with the invention, dilution of the first stage is carried out in tubes $11a_{1,1}, 11a_{1,2}, 11a_{4,1}, 11a_{4,2} \dots$ of the tube bank 11 through valves $V_1, V_2, V_3\dots$. White water is passed from a white water inlet header J_2 (arrow L_1) into tubes $D_1, D_2, D_3\dots$ and through them into the valves $V_1, V_2, V_3\dots$ and further through said adjustable valves $V_1, V_2 \dots$ into the tubes $11a_{1,1}, 11a_{1,2}, 11a_{4,1}, 11a_{4,2} \dots$ of the tube bank 11. The valves $V_1, V_2, V_3\dots$ are located, for example, with a spacing of 120 mm in connection with the headbox having a width of 10 m. The second dilution location, i.e. valves $V'_1, V'_2\dots$ of the second dilution
20 stage II are advantageously located in connection with turbulence pipes $13a_{1,1}, 13a_{1,2}, 13a_{1,3}, 11a_{2,1}, 13a_{2,2}, 13a_{2,3}$ of the turbulence generator 13 at different points of width across the headbox. Raw water is passed (arrow L_2) from a raw water inlet header J_3 into a duct $D'_1, D'_2, D'_3\dots$ and through the valves $V'_1, V'_2\dots$ further into the pipes $13a_{1,1}, 13a_{1,2}, 13a_{1,3}, 11a_{2,1}, 13a_{2,2}, 13a_{2,3}$ of the turbulence generator 13, in which the raw
25 stage employs fibre-free dilution water, an overall end result is achieved in which the accuracy of control is better than in conventional single-stage dilution and in which the construction costs with respect to structure have, however, not increased as compared with single-stage dilution.

water is passed into connection with the stock diluted in the first stage. The flow of the stock M_1 is denoted with the arrows S_1 and the flow of the dilution waters is denoted with the arrows L_1 and L_2 .

When the dilution liquid is passed into connection with the stock flow in the first
5 dilution stage and in the second stage, the dilution water is passed in the first
dilution stage I either into one or more, advantageously all tubes of the tube row of
the tube bank 11 at the width point in question. Similarly, in the second dilution
stage II, the dilution water can be passed either into one tube of the turbulence
generator 13 at the width point in question or into more tubes, advantageously into
10 all tubes at the width point in question.

CLAIMS

See Preliminary Amendment filed simultaneously herewith for claims.